# Polyethyleneimine entwine thermallytreated Zn/Co zeolitic imidazolate frameworks to enhance CO<sub>2</sub> adsorption

1<sup>st</sup> Jun Cheng<sup>\*</sup> State Key Laboratory of Clean Energy Utilization, Zhejiang University Hangzhou, China juncheng@zju.edu.cn 2<sup>nd</sup> Niu Liu State Key Laboratory of Clean Energy Utilization, Zhejiang University Hangzhou, China liuniu19961215@163.com 3<sup>rd</sup> Leiqing Hu<sup>1,2</sup> State Key Laboratory of Clean Energy Utilization, Zhejiang University Hangzhou, China leiqinghu@zju.edu.cn

Abstract-In order to solve the problems of deficient CO2 adsorption sites on Zn/Co zeolitic imidazolate frameworks(ZIFs), Zn/Co ZIFs were thermally treated to promote physical adsorption sites on Zn-N and Co-N bonds and then impregnated with polyethyleneimine (PEI) to promote -NH- and -NH<sub>2</sub>- chemical adsorption sites. The  $CO_2$  adsorption capacity detected on Micromeritics ASAP 2020C increased by 53% to 1.07mmol/g at 298K and 1bar, when Zn/Co ZIF was treated at optimal temperature of 450 °C to obtain the maximum Me-N2 unsaturated adsorption sites. This was because of a partial cleavage of coordination bonds between Zn-N, Co-N, C=N and C-N along with dissociation of rationally free methyl groups in the framework ligands, which was supported on density functional theory (DFT) calculation. The Zn/Co ZIF treated at 450 °C and then impregnated with 40wt% PEI exhibited the highest CO<sub>2</sub> adsorption capacity of 1.82 mmol/g under the condition of at 298K and 1bar, which was 2.6 times higher than that of raw Zn/Co ZIF. In addition, this adsorbent is proved to be regenerable and stable during 9 cycle CO<sub>2</sub> adsorptiondesorption tests, therefore, PEI- thermally treated Zn/Co ZIF exhibits a very promising application in CO<sub>2</sub> capture from flue gas and natural gas.

Keywords—CO<sub>2</sub> capture, adsorption, ZIF, PEI

## I. INTRODUCTION

The rapid development of global industrialization has resulted in growing concentrations of carbon dioxide(CO<sub>2</sub>) in the atmosphere, which has become a major environment problem[1] CO<sub>2</sub> is traditionally removed in gas purification application by using alkanolamines, such as monoethanolamine(MEA)[2], diethanolamine(DEA)[3], and methyldiethanolamine(MDEA)[4, 5].However, this chemical absorption technology suffers from high regenerative energy consumption, solvent loss, and corrosion, which hinders extensive application[6]. Thus, it is crucial to develop innovative sorbent materials achieving efficient separation of CO<sub>2</sub>.

Recently, a new class of microporous solid materials known as metal organic framework (MOFs) have emerged as potential adsorbents for effective separation and purification of gas mixtures[7-9].Despite the high number of novel MOFs synthesized, only a very limited number of them display satisfactory CO<sub>2</sub> capture performance at low pressure or ambient temperature because of the weak interaction between CO<sub>2</sub> and framework structure[10, 11]

Post-synthetic amine functionalization has been shown to be effective in improving the  $CO_2$ adsorption capacity of MOFs by exploiting the high affinity between  $CO_2$  and the amine groups[12-14]. Functionalization of magnesium-based MOFs with diamines has been widely reported to improve the CO<sub>2</sub> working capacity of the solids while increasing their CO<sub>2</sub>/N<sub>2</sub> selective factor compared with their unmodified counterpart[15, 16]. Zeolitic imidazolate frameworks(ZIFs), a MOF sub-family containing a sodalite-type cage similar to zeolites and imidazole bridging with the metallic node(e.g., Zn and Co)[7], have high thermal dynamic stability, chemical and moisture stability. Dual metal Zn/Co ZIFs is a sub-family in ZIFs that is constructed by an easy and straightforward room temperature technique using both  $Zn(NO_3)_2$  and  $Co(NO_3)_2$  as the metal precursors and 2-methylimidazole as the linker [7]. Besides, the preparation of ZIFs is more convenient for large-scale industrial CO2 removal applications[18]. The only drawback of ZIFs is the lower CO<sub>2</sub> working capacity compared to the topperforming MOFs. Hence, it is important to enhance the CO<sub>2</sub> adsorption capacity of ZIFs via amine functionalization. To the best of our knowledge, the literature on this approach is scare in last decade. Xian et al. synthesized novel PEIimpregnated ZIF-8 (PEI@ZIF-8) composites for CO<sub>2</sub>/N<sub>2</sub> separation[19]. In addition to post-synthetic amine modification of MOFs, the CO2 adsorption capacity of MOFs can be also increased by some simple methods. In 2014, Srinivas Gadipelli et al.

modified the structure of ZIF-8 by conducting a thermal treatment in a nitrogen atmosphere. This treatment resulted in the  $CO_2$  adsorption capacity of ZIF-8 increasing from 0.7 mmol/g to 1.79 mmol/g (1bar, 298K) [21].

In this study, a novel PEI-thermally treated Zn/Co ZIF adsorbent was synthesized by impregnation of PEI (MW=600g/mol) on Zn/Co ZIF adsorbents thermally treated at specific temperatures. The effect of the treatment temperature on the CO<sub>2</sub> working capacity of Zn/Co ZIF was revealed by XPS, FTIR, XRD and SEM analysis. Subsequently, PEI was impregnated on the samples in varying amounts and the CO<sub>2</sub> adsorption isotherms were obtained.

### II. Figures and Tables

Fig. 1 shows the  $N_2$  adsorption-desorption isotherms and the BJH pore size distributions of the Zn/Co ZIF samples treated at various temperatures. The BET surface areas of the Zn/Co ZIF samples treated at 400, 450, 500 °C were 1257, 1063, and 158 m<sup>2</sup>/g, respectively, while the mean pore size were 2.23, 2.72 and 9.77nm, respectively. The SEM images of the raw Zn/Co ZIF, Zn/Co ZIF treated at various temperatures and PEI impregnate treated Zn/Co ZIF sample are given in Fig.2. The Zn/Co ZIF particles were regular dodecahedron and the particle diameter ranged from 100 to 120nm. SEM images confirm that PEI was successfully loading on the Zn/Co ZIF particles.



Figure 1  $N_2$ -adsorption desorption isotherm (A) and pore size distributions (B) of Zn/Co ZIF adsorbents treated at various temperature.



(a) raw Zn/Co ZIF



(b) Zn/Co ZIF treated at 450°C



c) Zn/Co ZIF treated at 500°C

(d) Zn/Co ZIF (treated at 450°C) impregnated with polyethyleneimine (PEI) Fig 2. SEM images of Zn/Co ZIF adsorbents treated at various

Fig 2. SEM images of Zn/Co ZIF adsorbents treated at various temperatures

In order to obtain the optimum temperature for treating the Zn/Co ZIF samples, three different temperatures (400, 450, and 500 °C) were used for the initial Zn/Co ZIF. The CO<sub>2</sub> adsorption isotherms of the samples were measured at 298 K, Fig. 3 (a). Undoubtedly, the optimized structure of Zn/Co ZIF samples after the thermal treated produced a remarkable enhancement of the CO<sub>2</sub> adsorption capacity. MOFs having open metal centers (such as Mg-MOF-74 and, HKUST-1) exhibited significantly higher working capacities compared to fully coordinated metal MOFs (e.g., ZIF-8, ZIF-67, and MOF-5)[12,16]. The metals (Zn or Co) in the raw Zn/Co ZIF were fully coordinated (Me-N4, each metal center coordinate to four nitrogen atoms of four discrete ligands). After the thermally treated, part of the Zn-N and Co-N bonds were broken, and the bonding mode between the metal and nitrogen shifted from Me-N4 to Me-N2 (each metal center coordinated to two nitrogen atoms of two discrete ligands). Hence, the enhancement of the CO<sub>2</sub> working capacity for Zn/Co ZIF after the thermal treatment could be mainly explained by the presence of exposed Zn and Co sites[20]. The CO2 adsorption capacity of the Zn/Co ZIF sample treated at 450 °C increased by 53% (from 0.70 mmol/g to 1.07 mmol/g) compared to the raw Zn/Co ZIF. As the treated temperature increased to 500  $^{\circ}$ C, the framework decomposed and this was reveal by the marked reduction of the  $CO_2$  uptake, (only 0.75mmol/g at 298 K and, 1 bar). This high temperature let to the decomposition of the main framework structure, negatively affecting the CO<sub>2</sub> adsorption performance. Fig. 3 (b) shows the  $CO_2$  adsorption isotherm of PEI-thermally treated Zn/Co ZIF samples with different loadings measured by our homemade experiment instrument at 298 K and, 1bar. CO<sub>2</sub> adsorption capacity of the samples first increased and then decreased with the increasing of PEI loading. The CO<sub>2</sub> working capacity of the 20, 30, 40, 50, 60 wt% PEI impregnated samples were 1.27mmol/g(0.27mol CO<sub>2</sub>/mol NH<sub>2</sub> group), 1.48mmol/g(0.21mol CO<sub>2</sub>/ mol NH<sub>2</sub> group), 1.82 mmol/g (0.20mol CO<sub>2</sub>/ mol NH<sub>2</sub> group), 1.39mmol/g(0.12mol CO<sub>2</sub>/mol NH<sub>2</sub> group), 1.35mmol/g(0.10mol CO<sub>2</sub>/ mol NH<sub>2</sub>) group, respectively, exhibiting higher working capacities than the non-impregnated samples.



Fig.3 CO<sub>2</sub> adsorption isotherms (at 298 K): Zn/Co ZIF adsorbents treated at various temperatures(a), Zn/Co ZIF adsorbents (treated at 450  $^{\circ}$ C) impregnated with polyethyleneimine (PEI) (b)

#### III Conclusions and recommendations

A novel PEI- thermally treated Zn/Co ZIF adsorbent through postsynthetic functionalization was synthesized for the capture of CO<sub>2</sub>. This solid was firstly treated below the decomposition temperature and then functionalized with amine groups (PEI) to enhance the CO<sub>2</sub> working capacity. The CO<sub>2</sub> adsorption capacity of Zn/Co ZIF improved significantly(by 53%), from 0.7 mmol/g of raw Zn/Co ZIF to 1.07 mmol/g at 1bar and 298K, under the optimal treatment temperature condition at 450 °C. The CO<sub>2</sub> working capacity increased with PEI loading and reached a maximum for 40wt% PEI (1.82mmol/g at 298 K, 1 bar), 2.6 times higher than that of the raw Zn/Co ZIF.

#### ACKNOWLEDGEMENT

This work was supported by the National key research and development program- China (2016YFE0117900), National Natural Science Foundation-China (51676171), Zhejiang Provincial Key Research and Development Program-China (2017C04001).

#### REFERENCES

[1] K. Li, J. Jiang, F. Yan, S. Tian, X. Chen, The influence of polyethyleneimine type and molecular weight on the  $CO_2$  capture performance of PEI-nano silica adsorbents, Appl Energ 136 (2014) 750-755.

[2] U.E. Aronu, S. Gondal, E.T. Hessen, T. Haug-Warberg, A. Hartono, K.A. Hoff, H.F. Svendsen, Solubility of CO<sub>2</sub> in 15, 30,

45 and 60 mass% MEA from 40 to 120 °C and model representation using the extended UNIQUAC framework, Chem Eng Sci 66 (2011) 6393-6406.

[3] Y. Choi, N. Zhang, P. Zhou, Efficiency and abatement costs of energy-related CO<sub>2</sub> emissions in China: A slacks-based efficiency measure, Appl Energ 98 (2012) 198-208.
[4] N. Rodr guez, S. Mussati, N. Scenna, Optimization of post-combustion CO<sub>2</sub> process using DEA–MDEA mixtures, Chemical Engineering Research and Design 89 (2011) 1763-1773.

[5] X. Zhang, C.-F. Zhang, Y. Liu, Kinetics of Absorption of  $CO_2$  into Aqueous Solution of MDEA Blended with DEA, Ind Eng Chem Res 41 (2002) 1135-1141.

[6] J. Cheng, Y. Li, L. Hu, J. Liu, J. Zhou, K. Cen, CO<sub>2</sub> absorption and diffusion in ionic liquid [P66614][Triz] modified molecular sieves SBA-15 with various pore lengths, Fuel Process Technol 172 (2018) 216-224.

[7] K. Zhou, B. Mousavi, Z. Luo, S. Phatanasri, S. Chaemchuen, F. Verpoort, Characterization and properties of Zn/Co zeolitic imidazolate frameworks vs. ZIF-8 and ZIF-67, J Mater Chem A 5 (2017) 952-957.

[8] K. Adil, P.M. Bhatt, Y. Belmabkhout, S.M.T. Abtab, H. Jiang, A.H. Assen, A. Mallick, A. Cadiau, J. Aqil, M. Eddaoudi, Valuing Metal–Organic Frameworks for Postcombustion Carbon Capture: A Benchmark Study for Evaluating Physical Adsorbents, Advanced Materials 29 (2017) 1702953.

[9] Z. Zhang, Z.-Z. Yao, S. Xiang, B. Chen, Perspective of microporous metal–organic frameworks for CO<sub>2</sub> capture and separation, Energ Environ Sci 7 (2014) 2868-2899.

[10] P. Nugent, Y. Belmabkhout, S.D. Burd, A.J. Cairns, R. Luebke, K. Forrest, T. Pham, S. Ma, B. Space, L. Wojtas, M. Eddaoudi, M.J. Zaworotko, Porous materials with optimal adsorption thermodynamics and kinetics for CO<sub>2</sub> separation, Nature 495 (2013) 80.

[11] T.M. McDonald, J.A. Mason, X. Kong, E.D. Bloch, D. Gygi, A. Dani, V. Crocell à F. Giordanino, S.O. Odoh, W.S. Drisdell, B. Vlaisavljevich, A.L. Dzubak, R. Poloni, S.K. Schnell, N. Planas, K. Lee, T. Pascal, L.F. Wan, D. Prendergast, J.B. Neaton, B. Smit, J.B. Kortright, L. Gagliardi, S. Bordiga, J.A. Reimer, J.R. Long, Cooperative insertion of CO<sub>2</sub> in diamine-appended metal-organic frameworks, Nature 519 (2015) 303.

[12] R. Vaidhyanathan, S.S. Iremonger, K.W. Dawson, G.K.H. Shimizu, An amine-functionalized metal organic framework for preferential CO<sub>2</sub> adsorption at low pressures, Chemical Communications (2009) 5230-5232.

[13] R.L. Siegelman, T.M. McDonald, M.I. Gonzalez, J.D. Martell, P.J. Milner, J.A. Mason, A.H. Berger, A.S. Bhown, J.R. Long, Controlling Cooperative CO<sub>2</sub> Adsorption in Diamine-Appended Mg<sub>2</sub>(dobpdc) Metal–Organic Frameworks, J Am Chem Soc 139 (2017) 10526-10538.

[14] T.M. McDonald, W.R. Lee, J.A. Mason, B.M. Wiers, C.S. Hong, J.R. Long, Capture of Carbon Dioxide from Air and Flue Gas in the Alkylamine-Appended Metal–Organic Framework mmen-Mg2(dobpdc), J Am Chem Soc 134 (2012) 7056-7065.
[15] W.R. Lee, H. Jo, L.-M. Yang, H. Lee, D.W. Ryu, K.S. Lim, J.H. Song, D.Y. Min, S.S. Han, J.G. Seo, Y.K. Park, D. Moon, C.S. Hong, Exceptional CO<sub>2</sub> working capacity in a

heterodiamine-grafted metal–organic framework, Chemical Science 6 (2015) 3697-3705.

[16] J.S. Yeon, W.R. Lee, N.W. Kim, H. Jo, H. Lee, J.H. Song, K.S. Lim, D.W. Kang, J.G. Seo, D. Moon, B. Wiers, C.S. Hong, Homodiamine-functionalized metal–organic frameworks with a MOF-74-type extended structure for superior selectivity of  $CO_2$  over N2, J Mater Chem A 3 (2015) 19177-19185.

[17] X. Su, L. Bromberg, V. Martis, F. Simeon, A. Huq, T.A. Hatton, Postsynthetic Functionalization of Mg-MOF-74 with Tetraethylenepentamine: Structural Characterization and Enhanced CO<sub>2</sub> Adsorption, ACS Applied Materials & Interfaces 9 (2017) 11299-11306.

[18] Z. Zhang, S. Xian, Q. Xia, H. Wang, Z. Li, J. Li, Enhancement of CO<sub>2</sub> Adsorption and CO<sub>2</sub>/N<sub>2</sub> Selectivity on ZIF-8 via Postsynthetic Modification, AIChE Journal 59 (2012) 2195-2206.

[19] S. Xian, F. Xu, C. Ma, Y. Wu, Q. Xia, H. Wang, Z. Li, Vapor-enhanced CO<sub>2</sub> adsorption mechanism of composite PEI@ZIF-8 modified by polyethyleneimine for CO2/N2 separation, Chemical Engineering Journal 280 (2015) 363-369.

[20] J. Pokhrel, N. Bhoria, S. Anastasiou, T. Tsoufis, D. Gournis, G. Romanos, G.N. Karanikolos, CO2 adsorption behavior of amine-functionalized ZIF-8, graphene oxide, and ZIF-8/graphene oxide composites under dry and wet conditions, Micropor Mesopor Mat 267 (2018) 53-67.