

EFFECT OF CaO/Fe₂O₃ ON SLAG VISCOSITY BEHAVIOR UNDER ENTRAINED FLOW GASIFICATION CONDITIONS

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ABSTRACT

The entrained flow gasification is becoming a predominant and efficient way for coal clean utilization. And the steady and reliable removal of the ash slag is the key factor for smooth operation of entrained gasifiers. For the purpose of reducing the additive amount of flux and improving gasification efficiency, the influence of CaO/Fe₂O₃ (weight ratio of CaO/Fe₂O₃) on the viscosity-temperature behavior was studied in this work. Slag structure at high temperatures, and crystallization behavior of the coal ash slag with different CaO/Fe₂O₃ were studied in detail. As the CaO/Fe₂O₃ of the slag decreased, viscosity of the slag decreased at same temperatures. And Fe₂O₃ has a more decreasing effect on slag viscosity compared with CaO. Si-O-Si proportion is the key factor to influence slag viscosity when CaO/Fe₂O₃ is over 6:4, for other CaO/Fe₂O₃, Al-O structure should be considered. Both positive and negative mutual effect exist between CaO and Fe₂O₃. When CaO/Fe₂O₃ is lower than 2:8, they have negative mutual effect for breaking Si-O-Si bond. In addition, Sample 10C0F and 2C8F are suitable for the smooth operation of entrained flow gasification.

Keywords: Entrained flow gasification; Slag viscosity behavior; CaO/Fe₂O₃; Network structure; Crystallization

1. INTRODUCTION

The efficient and clean utilization of the coal is increasingly urgent for sustainable development [1]. Coal gasification is becoming the main clean coal utilization technology. Typically, based on the flow mechanism of Selection and peer-review under responsibility of the scientific committee of the 11th Int. Conf. on Applied Energy (ICAE2019).
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feedstock, coal gasification technology can be divided into fixed bed, fluid bed and entrained flow gasification [2]. The last one has becoming the most promising choice for the advantages of high throughput, high carbon conversion and fuel feedstock flexibility [3].

The entrained flow gasifier is slagging gasifier, the smooth slag tapping is the key factor to ensure long-term operation of the gasifier, which is largely dependent on slag viscosity behavior [4]. Therefore, the slag viscosity behavior becomes the first principle for smooth operation of the entrained flow gasification.

Most of coals in China are not suitable for slag tapping because of the high slag viscosity at high temperatures [5]. To broaden the range of coals that can be processed in entrained flow slagging gasifiers, the fluxes which usually contains network modifiers are always used to blend the feedstock to produce a feed with appropriate slag viscosity behavior [6].

In this work, the viscosity behavior of the slags with same CaO+Fe₂O₃ content, different CaO/Fe₂O₃ were proceeded to investigate the mutual effect of different metal oxides. The structure of molten slags was studied by solid-state nuclear magnetic resonance (SS-NMR) and Raman. In addition, the crystallization behavior of the slags was analyzed by thermochemical calculation and the mineral compositions were studied by X-ray diffraction (XRD).

2. MATERIAL AND METHODS

2.1 Synthetic ash materials

To eliminate negative impact caused by irrelevant elements, the ash samples were simplified via using the

synthetic ash. The ashes were composed of $\text{SiO}_2\text{-Al}_2\text{O}_3\text{-Na}_2\text{O-CaO-Fe}_2\text{O}_3$, which accounted for more than 90% (mass fraction) in a real coal ash. Analytic reagents SiO_2 , Al_2O_3 , Fe_2O_3 , CaO were chosen and Na_2CO_3 instead of Na_2O was selected. These five reagents were ground to less than $75\ \mu\text{m}$ (200 mesh) and then mixed thoroughly in a ball milling. Chemical compositions of the synthetic ashes are listed in Table 1. The samples had same Si/Al (1.5) (mass ratio of $\text{SiO}_2/\text{Al}_2\text{O}_3$), Si+Al (65%) (total content of $\text{SiO}_2+\text{Al}_2\text{O}_3$), and same $\text{CaO}+\text{Fe}_2\text{O}_3$ (34%) (total content of $\text{CaO}+\text{Fe}_2\text{O}_3$), but different $\text{CaO}/\text{Fe}_2\text{O}_3$ (mass ratio of $\text{CaO}/\text{Fe}_2\text{O}_3$).

Table 1 Chemical compositions of the materials (wt%)

Sample	SiO_2	Al_2O_3	Na_2O	CaO	Fe_2O_3
10COF ¹	39.0	26.0	1.0	34.0	0.0
8C2F ²	39.0	26.0	1.0	27.2	6.8
6C4F	39.0	26.0	1.0	20.4	13.6
4C6F	39.0	26.0	1.0	13.6	20.4
2C8F	39.0	26.0	1.0	6.8	27.2
0C10F	39.0	26.0	1.0	0.0	34.0

¹: 10COF: 34% (mass fraction) CaO in the synthetic ash without Fe_2O_3 ;

²: 8C2F: mass ratio of CaO and Fe_2O_3 is 8:2.

2.2 Viscosity measurement

About 100-105 g the synthetic ash samples were firstly heated to $150\ ^\circ\text{C}$ higher than T_{liq} and hold for 20 min to reach the equilibrium in an electric furnace. After that, part of the pre-melted slags was broken to less than 2 mm and others were ground to less than $75\ \mu\text{m}$ for quenched experiment.

Viscosity measurement was performed by a Theta high temperature rotational viscometer (RV DV-III). About 50 g pre-melted slags were put into an alumina crucible and then fixed at the center of the furnace. The protect alumina tube was evacuated fully and a reducing atmosphere ($\text{CO}/\text{CO}_2=6:4$, volume fraction) was used to blow the slag sample with a rate of 50 ml/min. The furnace was gradually heated to $1200\ ^\circ\text{C}$ at $10\ ^\circ\text{C}/\text{min}$ and then to $1600\ ^\circ\text{C}$ at $5\ ^\circ\text{C}/\text{min}$. To ensure the melting of all crystalline solids, this temperature was hold for 20 min. Then, the spindle was immersed into the molten slag and the measurement started at a cooling rate of $3\ ^\circ\text{C}/\text{min}$ at a constant share rate of $2.5\ \text{s}^{-1}$. The slag viscosity and temperature were recorded at the interval of $0.1\ ^\circ\text{C}$.

2.3 Preparation of quenched slag

A horizontal electricity tube furnace was used to prepare quenched slags under a reducing atmosphere as viscosity measurements. The temperature program in quenching experiment was same with that in viscosity measurement. When the temperature was decreased to the set point, the ash sample was pulled out rapidly and quenched in ice water immediately. All quenched slag samples were crushed and ground to less than $75\ \mu\text{m}$ for XRD analysis, Raman and NMR characterization.

2.4 Characterization of quenched slags

Quenched slag at $1500\ ^\circ\text{C}$ (1773K , $>T_{\text{liq}}$) was chosen to analyze the structure of molten slag by Raman characterization. The quenched slags were ground to less than $75\ \mu\text{m}$. A Horiba LabRAM HR800 spectrometer equipped with a CCD detector was carried out to analyze the coordination of Si atoms. The $514.5\ \text{nm}$ line of an Ar+ laser was used for sample excitation.

²⁷Al MAS-NMR spectra were measured at a Bruker Avance III 600 MHz Wide Bore spectrometer (magnetic field 14.1 T) using a 4 mm CPMAS probe under 13 kHz MAS speed in zirconia rotors. ²⁷Al radiofrequency field strength was verified by using a 1.0 M aqueous AlCl_3 solution. Chemical shift was referenced to the AlCl_3 signal.

To investigate mineral compositions of slag samples during cooling, a Bruker D2 X-ray powder diffractometer with $\text{Cu K}\alpha$ radiation (40 kV, 40 mA) was employed. The quenched slags were placed on a sample stage and scanned with a step size of 0.02° at $4^\circ/\text{min}$ range from 5° to 90° (2θ).

2.5 Thermal calculation

FactSage software is widely used to predict the equilibration of multiphase, liquidus temperature as well as the proportion of slag and solid. In this study, the FToxide and FactPs database were selected to calculate the phase diagram.

2.6 Results and Discussion

2.6.1 High-temperature viscosity behavior

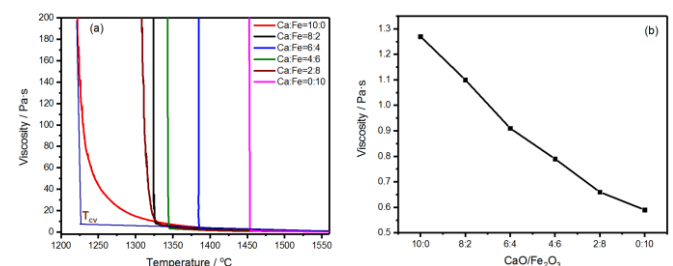


Fig. 1 (a) Viscosity-temperature curves of the ash slags with different $\text{CaO}/\text{Fe}_2\text{O}_3$

(b) Slag viscosity value at 1500 °C

From Fig. 1(a), as CaO/Fe₂O₃ decreased, the slag viscosity value at same temperatures decreased, and the difference of the slag viscosity was more obvious at low temperatures. For example, at 1500 °C, the viscosity values were 1.27, 1.1, 0.91, 0.79, 0.66, 0.59 Pa·s respectively for the sample from 10C0F to 0C10F. This suggested that Fe₂O₃ has a more decreasing effect on slag viscosity compared with CaO.

It also can be observed that the slag contained Fe₂O₃ exhibited crystal behavior, while sample 10C0F behaved as a glassy slag. The rapid increase of viscosity was usually attributed to the formation of the crystalline phases. This implies that the decrease of CaO/Fe₂O₃ is benefit to forming crystalline phases during cooling.

Slag structure and crystallization behavior were main factors which affect slag viscosity-temperature behavior. Therefore, the effect of CaO/Fe₂O₃ on slag structure and crystallization behavior was investigated and discussed in the following study.

2.6.2 Effect of CaO/Fe₂O₃ on Si-O structure

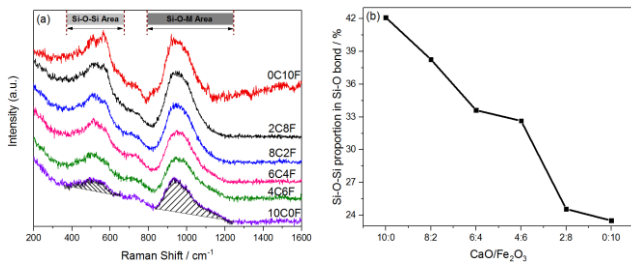


Fig. 2 (a) Raman spectra of the quenching ash slags at 1500 °C (b) Si-O-Si bond proportion among all Si-O bonds

From Fig. 2(a), the raman shift of 400-600 cm⁻¹ was assumed as Si-O-Si bond, and the range of 800-1200cm⁻¹ was defined as Si-O-M (Al, Ca, Fe, Na) bonds. The calculated Si-O-Si proportion was presented in Fig 2(b). The results showed that with decreasing CaO/Fe₂O₃, Si-O-Si ratio decreased, which caused low polymerization degree of molten slag. Consequently, a low viscosity value was obtained at high temperatures.

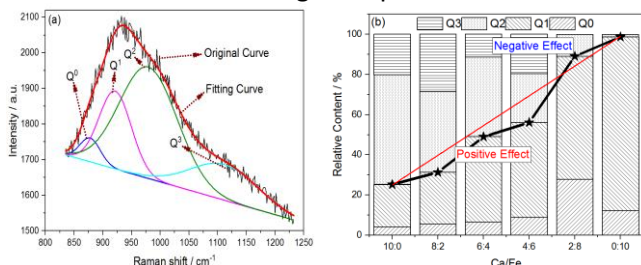


Fig. 3 (a) A typical deconvolution of raman spectra (b) Contents of Qⁿ units based on deconvolution results

In Fig. 3(a), to further investigate the influence of CaO/Fe₂O₃ on Si-O-M bonds (Q⁰, Q¹, Q², Q³ species), the method of deconvolution was applied to analyze the

extensively overlapped individual peak by gaussian method around 800-1200 cm⁻¹. The results was depicted in Fig 3(b). With decreasing Ca/Fe, Q⁰+Q¹ contents increased, which meant ferrous ion has higher ability to break Si-O-Si bond than Ca²⁺. As for breaking Si-O-Si bond, when CaO/Fe₂O₃ is over 4:6, CaO and Fe₂O₃ has a positive mutual effect. While the ratio is less than 2:8, CaO and Fe₂O₃ has a negative mutual effect.

2.6.3 Effect of CaO/Fe₂O₃ on Al-O structure

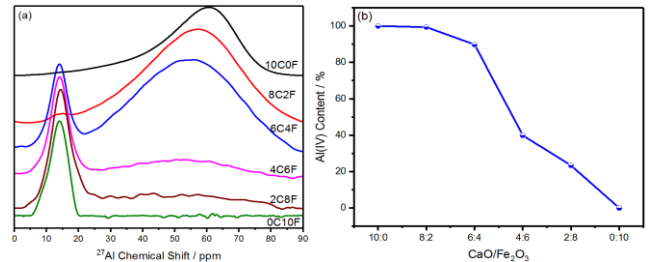


Fig. 4 (a) ²⁷Al NMR spectra of quenching ash slags at 1500 °C (b) Al(IV) content as a function of CaO/Na₂O

The influence of CaO/Fe₂O₃ on Al-O structure was also discussed, and the results were drawn in Fig. 4. Generally, the range around 50-100 ppm was Al-IV ([AlO₄]⁵⁻, tetrahedron structure) and the range around 10-20 ppm was responsive for Al-VI ([AlO₆]⁹⁻, octahedral structure). It can be observed that chemical shift of [AlO₄]⁵⁻ moved to lower frequency with the decreasing CaO/Fe₂O₃. And Al-VI structure appeared gradually with decreasing CaO/Fe₂O₃, while Al-IV vanished gradually. From Fig. 4(b), Al-IV content decreased with decreasing CaO/Fe₂O₃. The results indicated that low CaO/Fe₂O₃ was benefit for the formation of Al-VI, which decomposed slag polymerization degree, resulting in low viscosity.

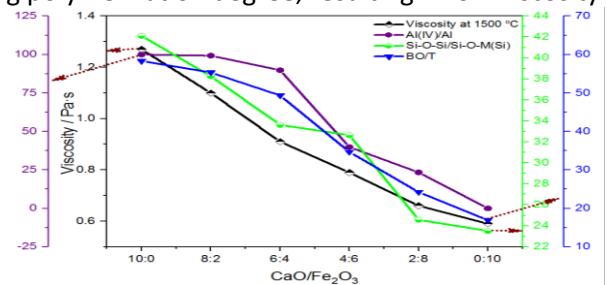


Fig. 5 Correlation between slag viscosity and Al-IV proportion, Si-O-Si proportion, BO/T (considering both Si-O and Al-O)

To further illustrate the main aspect for influencing slag viscosity at high temperatures. The relationship between three slag structure parameters tested by quenching slag at 1500 °C and slag viscosity value at 1500 °C was shown in Fig. 5. All the curves had same tendency. However, when CaO/Fe₂O₃ is over 6:4, slag viscosity was mainly determined by Si-O structure. While CaO/Fe₂O₃ is lower than 4:6, BO/T is the main parameter to influence slag viscosity due to the change on Al-O structure caused

