

1. INTRODUCTION

The CCS technology was first evolved by American oil companies using CO₂ to drive oil to improve oil recovery in the 1970s. After more than 50 years of development, CCS technology has gradually developed into a key measure to curb greenhouse gas emissions [1]. CCS includes three links: CO₂ capture, transportation and storage, that is, first separate and capture CO₂, then select transportation tools to send to appropriate storage sites, and finally use or inject underground, oil (gas) displacement, mineralization and other permanent storage, followed by long-term monitoring and management [2]. At present, CO₂ geological storage methods mainly include: injecting oil and gas wells to improve oil and gas recovery, injecting coal seams to obtain methane, injecting waste oil and gas fields, underground salt water layer and seabed storage. However, in the current research on CCS technology, there are relatively few studies on CO₂, transportation and storage technology. The storage of CO₂ is affected by the properties of storage medium, temperature, pressure and clay minerals, as shown in Figure 1[3].

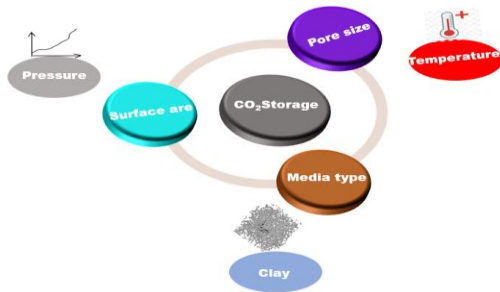


Fig 1 Schematic showing the complex relationship of impact factor and CO₂ storage in reservoir

The development difficulties of offshore heavy oil reservoirs are mainly deep buried reservoir, high porosity, fine lithology, thin single layer and complex oil-water relationship, resulting in high steam injection pressure, large heat loss, small steam spread range and poor development benefit, which makes CO₂ occupy a certain position in EOR of such reservoirs, which also provides good storage conditions for CO₂ storage [4].

2. METHODOLOGY

2.1 General assumptions

To illustrate the conditions for using the new model, the following basic assumptions are made:

(a) The oil layer is thick enough to ignore the heat loss to the surrounding formation;

(b) The rock reaches the fluid temperature instantaneously;

(c) The fluctuations of fluid properties and flow parameters along the horizontal section, such as temperature, pressure and steam quality, are ignored;

(d) The Free sand are oil wet particles.

2.2 Description of the model

The sand production model is revised, the traditional geomechanical model is transformed into a geochemical mechanism model, and the interaction between CO₂ and rock is considered in the sand production model, to store CO₂.

The mathematical description of CO₂ rock interaction is expressed by Arrhenius formula. CO₂ dissolves the reservoir rock under thermal conditions, and the dissolution process will cause the flow of reservoir solid phase, that is, the release of reservoir particles. The formula is as follows.

$$r = Ae^{\frac{-E_a}{RT}} C \quad (1)$$

The porous media contains fluids (water, oil, gas) which together fill the void space. These fluids are multicomponent mixtures. The equations of continuity for these species are [5]

$$\frac{\partial}{\partial t} (\phi x_{ij} S_j \rho) + \nabla \cdot (\phi x_{ij} S_j \rho v_j) = \dot{m} \quad (2)$$

In fact, as previous studies have shown, there is a critical flow rate in the model, beyond which failure can be expected. The coupling between the two failure mechanisms is mathematically expressed in the form of the above parameters. Porosity is selected as the coupling parameter. With the increase of porosity, it is assumed that the elasticity and strength (cohesion) of rock become weak.

$$\dot{m} = \beta(1-\phi)(v_f - v_{cr}) \quad (3)$$

$$\beta = \begin{cases} 0 & v_f \leq v_{cr} \\ r & v_f > v_{cr} \\ v_f & \end{cases} \quad (4)$$

The energy equation of steam injection is as follows

$$\frac{\partial T(\rho c)}{\partial x} - \nabla T \cdot (\rho c v_f)_w = \nabla \cdot \lambda_r \nabla T + q_L \quad (5)$$

The equation is a partial differential equation (PDE). The first term on the left side of PDE represents the accumulated heat in the reservoir, and the second term on represents thermal convection. For the previous model, the fluid velocity "V" is regarded as a constant value to avoid the complexity of solving partial differential equations. In fact, for flow in reservoir, the fluid velocity will gradually decrease with the increase of reservoir range. This term is modified by introducing a new thermal convection velocity, which varies with reservoir range. Therefore, a new energy conservation equation can be derived. In addition, the first item on the right represents heat conduction, and the second item on the right represents heat loss of surrounding layers [6].

Porosity change based on skeleton erosion is also the main result of CO₂ storage during cyclic steam stimulation in offshore heavy oil.

$$\phi(v_f - v_{cr}) = \frac{Kk}{\mu} \nabla p_j \quad (6)$$

2.3 Solving method

Thermal recovery is the main way of onshore heavy oil reservoir development. For offshore heavy oil fields, due to the limitation of platform space and high thermal recovery cost, the research in this field started late. At present, the evaluation of thermal recovery development effect of offshore heavy oil reservoir in the literature is mainly based on field pilot test analysis and numerical simulation analysis, but there are few achievements in production mechanism and experimental research, which makes the design of gas injection parameters lack of scientific.

The numerical model is shown in Figure 2 below. The length and width of the rectangle are 104 m, 42 m, respectively. The thickness of the rectangle is 24m. For a single microelement, the length and width are 2 m and 1 m, respectively, and the thickness is 2 m. the porosity of the reservoir is 0.37. The permeability in the I-direction is 2000 mD, and the permeability in the J- and K-directions are 2000 mD and 600 mD, respectively. The initial reservoir pressure is 2360 kPa. The initial reservoir temperature is 289K. the injection rate is 10 m³/day and the production pressures for the four producers are 101 kPa.

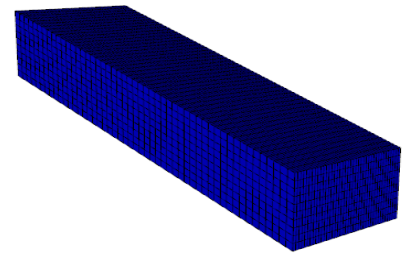


Fig 2 Model cotruction

3. RESULT AND DISCUSSION

3.1 Characteristics of edge water intrusion during steam huff and puff and gas injection

Figure 3 shows the oil saturation field of the mechanism model of offshore edge water heavy oil reservoir. The edge water intensity of this kind of reservoir is large. It can be seen from the figure that water invasion is very easy to occur. During the development process, the steam heat loss is large and the water breakthrough time is early. After three cycles of steam huff and puff, the edge water of the basic reservoir almost fills the bottom of the well, resulting in a decline in production. When the water cut exceeds 90%, CO₂ is injected into the reservoir, and then steam huff and puff is carried out, as shown in Fig. 5. It is obvious that the oil saturation at the bottom of the well increases and the edge water is controlled within a certain range. Therefore, CO₂ assisted steam huff and puff has a significant effect on water control and oil increase, especially for offshore edge water heavy oil reservoirs.

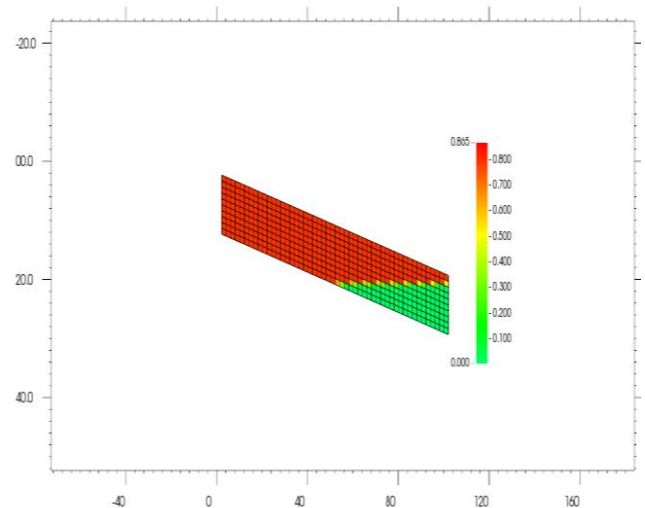


Fig 3 Initial oil saturation

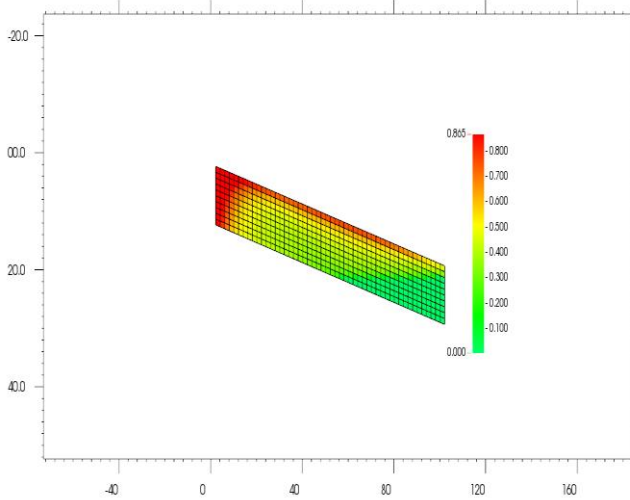


Fig 4 Oil saturation after 3 cycle of steam huff and puff

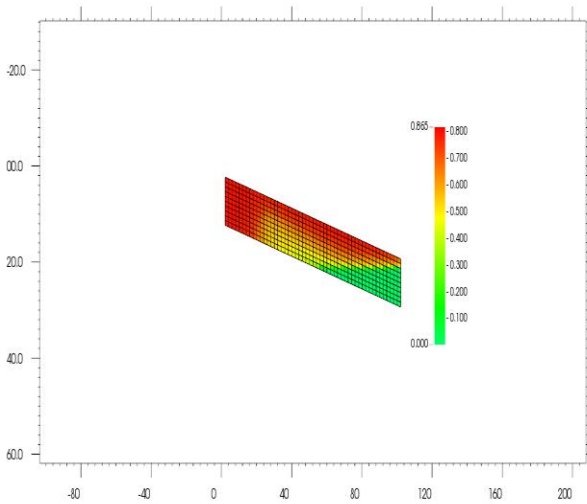


Fig 5 Oil saturation after CO₂ injection

3.2 Porosity change after gas injection

As shown in figures 6 and 7, CO₂ injection first acts with formation fluid to increase the elastic energy of crude oil on the one hand and supplement bottom hole energy on the other hand, to control the invasion of edge water. However, when the injection amount of CO₂ continues to increase, CO₂ will react with the reservoir rock to produce secondary pores, and lead to the weakening of the rock skeleton strength of the reservoir, so the initial pores change little. As shown in Fig. 8, when CO₂ injection is stopped and steam huff and puff production is carried out again, due to the decrease of CO₂ solubility under high temperature, a large amount of gas diffuses around the well, resulting in the increase of

dissolution pores, and particle migration with crude oil production and storage, resulting in the increase of porosity

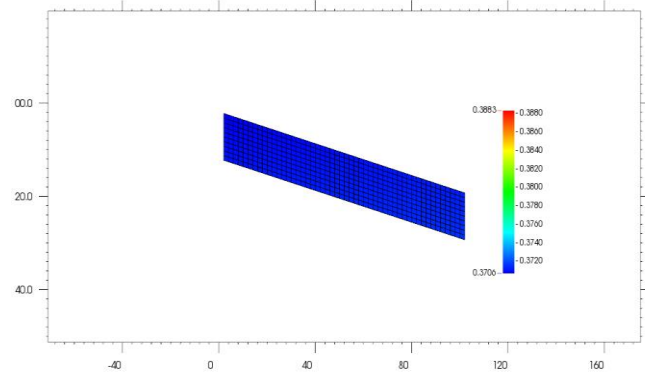


Fig 6 Initial Porosity

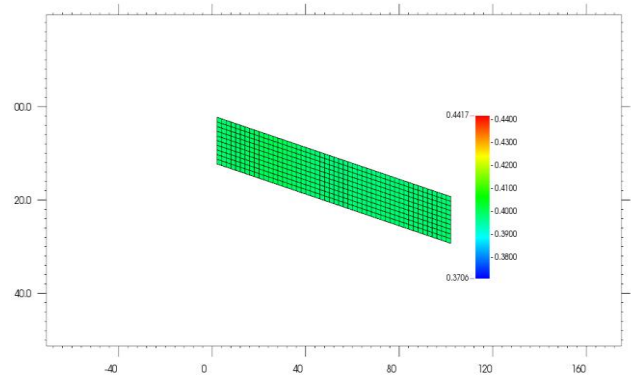


Fig 7 Porosity change during CO₂ injection

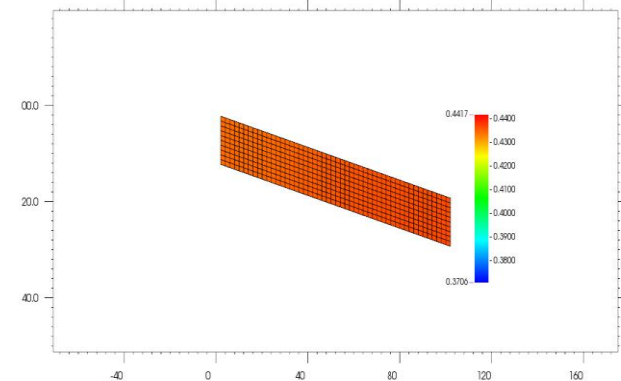
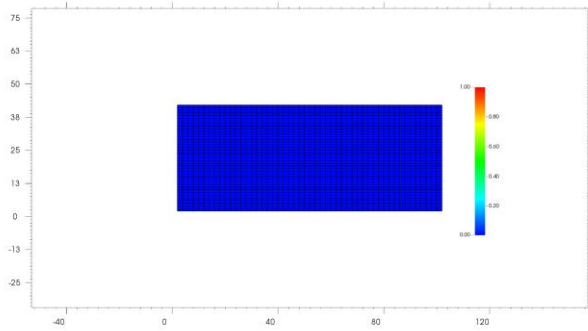
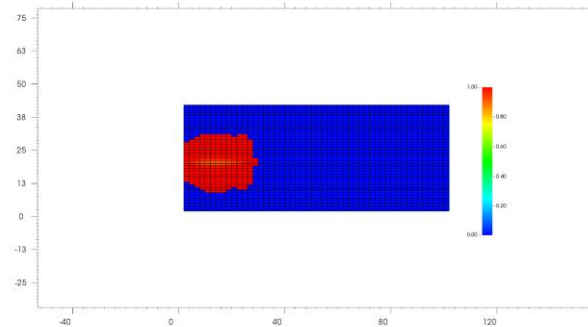
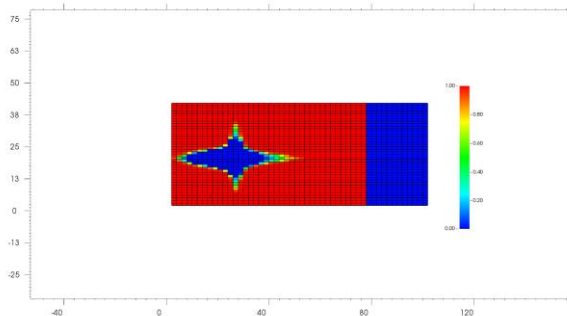


Fig 8 Porosity change during CO₂ injection with steam

3.3 Characteristics of CO₂ storage during steam huff and puff and gas injection

It can be seen from figure 9-10 that CO₂ injection can achieve the purpose of storage for offshore edge water reservoir. In addition, after heat injection, it will increase the hydrothermal effect of rock and the diffusion of CO₂ to deep layer, to improve the CO₂ storage efficiency.

Fig 9 CO₂ molar factorFig 10 CO₂ molar factor during soakFig 11 CO₂ molar factor after steam injection

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4. CONCLUSION

(1) Steam CO₂ slug injection has obvious effect on water control and oil increase, which is widely used in offshore edge water heavy oil reservoir.

(2) CO₂ first interacts with reservoir fluid and then with reservoir rock, besides, interaction of CO₂ and rock is the main principle of CO₂ storage.

(3) Temperature is conducive to CO₂ storage but not conducive to displacement oil efficiency. Therefore, integration of CO₂ storage and oil recovery is feasible for offshore strong edge water reservoirs.